where $h_{c}=$ heat-transfer coefficient by convection, $\mathrm{J} /\left(\mathrm{m}^{2} \cdot \mathrm{~s} \cdot \mathrm{~K}\right)$ [Btu/ $\left.\left(\mathrm{h} \cdot \mathrm{ft}^{2} \cdot{ }^{\circ} \mathrm{F}\right)\right] ; t=$ air temperature, $\mathrm{K} ; t_{w}=$ wet-bulb temperature of air, K ; $k_{g}^{\prime}=$ mass-transfer coefficient, $\mathrm{kg} /\left(\mathrm{s} \cdot \mathrm{m}^{2}\right)(\mathrm{kg} / \mathrm{kg})\left[\mathrm{lb} /\left(\mathrm{h} \cdot \mathrm{ft}^{2}\right)(\mathrm{lb} / \mathrm{lb})\right] ; \lambda=$ latent heat of evaporation at $t_{w}, \mathrm{~J} / \mathrm{kg}(\mathrm{Btu} / \mathrm{lb}) ; H_{w}=$ saturated humidity at $t_{w}=\mathrm{kg} / \mathrm{kg}$ of dry air; and $H_{a}=$ humidity of the surrounding air, $\mathrm{kg} / \mathrm{kg}$ of dry air.

For air-water-vapor mixtures, it so happens that $h_{c} / k_{g}^{\prime}=C_{s}$ approximately, although there is no theoretical reason for this. Hence, since the ratio $\left(H_{w}-H_{a}\right) /\left(t_{w}-t\right)$ equals $h_{c} / k_{g}^{\prime} / \lambda$, which represents the slope of the wet-bulb-temperature lines, it is also equal to $C_{s} / \lambda$, the slope of the adiabatic-saturation lines as shown previously.

A given humidity chart is precise only at the pressure for which it is evaluated. Most air-water-vapor charts are based on a pressure of 1 atm . Humidities read from these charts for given values of wet- and dry-bulb temperature apply only at an atmospheric pressure of 760 mmHg . If the total pressure is different from 760 mmHg , the humidity at a given wet-bulb and dry-bulb temperature must be corrected according to the following relationship.

$$
\begin{equation*}
H_{a}=H_{o}+0.622 p_{w}\left(\frac{1}{P-p_{w}}-\frac{1}{760-p_{w}}\right) \tag{12-23}
\end{equation*}
$$

where $H_{a}=$ humidity of air at pressure $P, \mathrm{~kg} / \mathrm{kg}$ of dry air; $H_{o}=$ humidity of air as read from a humidity chart based on $760-\mathrm{mm}$ pressure at the observed wet- and dry-bulb temperatures, $\mathrm{kg} / \mathrm{kg}$ dry air, $p_{w}=$ vapor pressure of water at the observed wet-bulb temperature, mmHg ; and $P=$ the pressure at which the wet- and dry-bulb readings were taken. Similar corrections can be derived to correct specific volume, the saturation-humidity curve, and the relative-humidity curves.

## HUMIDITY CHARTS FOR SOLVENT VAPORS

Humidity charts for other solvent vapors may be prepared in an analogous manner. There is one important difference involved, however, in that the wet-bulb temperature differs considerably from the adia-batic-saturation temperatures for vapors other than water.

Figures 12-37 to 12-39 show humidity charts for carbon tetrachloride, benzene, and toluene. The lines on these charts have been calculated in the manner outlined for air-water vapor except for the wet-bulb-temperature lines. The determination of these lines depends on data for the psychrometric ratio $h_{c} / k_{g}^{\prime}$, as indicated by Eq. (12-22). For the charts shown, the wet-bulb-temperature lines are based on the following equation:

$$
\begin{equation*}
H_{w}-H=\left(\alpha h_{c} / \lambda_{w} k_{g}^{\prime}\right)\left(t-t_{w}\right) \tag{12-24}
\end{equation*}
$$

where $\alpha=$ radiation correction factor, a value of 1.06 having been used for these charts. Values of $h_{c} / k_{g}^{\prime}$, obtained from values of $h_{c} / k_{g}^{\prime} C_{s}$ as presented by Walker, Lewis, McAdams, and Gilliland (Principles of Chemical Engineering, 3d ed., McGraw-Hill, New York, 1937), where $C_{s}=$ humid heat of air with respect to the vapor involved, are as follows:

| Material | Carbon <br> tetrachloride | Benzene | Toluene |
| :---: | :---: | :---: | :---: |
| $h_{c} / k_{g}^{\prime} C_{s}$ | 0.51 | 0.54 | 0.47 |

A discussion of the theory of the relationship between $h_{c}$ and $k_{g}^{\prime}$ may be found in the psychrometry part of this section. Because both theoretical and experimental values of $h_{c} / k_{g}^{\prime}$ apply only to dilute gas mixtures, the wet-bulb lines at high concentrations have been omitted. For a discussion of the precautions to be taken in making psychrometric determinations of solvent vapors at low solvent wet-bulb temperatures in the presence of water vapor, see the paper by Sherwood and Comings [Trans. Am. Inst. Chem. Eng., 28, 88 (1932)].

## GENERAL CONDITIONS FOR DRYING

Solids drying encompasses two fundamental and simultaneous processes: (1) heat is transferred to evaporate liquid, and (2) mass is


FIG. 12-37 Humidity chart for air-carbon tetrachloride vapor mixture. To convert British thermal units per pound to joules per kilogram, multiply by 2326 ; to convert British thermal units per pound dry air-degree Fahrenheit to joules per kilogram-kelvin, multiply by 4186.8; and to convert cubic feet per pound to cubic meters per kilogram, multiply by 0.0624 .

